

## DESCRIPTION AMENDMENTS

**After the title, insert the following new paragraph:**

This is a national stage application filed under 35 USC 371 based on International Application No. PCT/FI2004/050019 filed February 25, 2004, and claims priority under 35 USC 119 of Finnish Patent Application No. 20031848 filed December 18, 2003 and International Application No. PCT/FI2004/050009 filed January 30, 2004.

**Rewrite the paragraph beginning on page 9, line 23, to read as follows:**

Gas from the reservoir is led to the gas main supply line 7 via a second duct section 3.5 of the second gas supply line 3. When the output of the boil-off gas (first gas supply line 2) is not enough for consumption demand, the pressure in the main supply line 7 and also in the ullage space section of the cargo tank 4 will modestly decrease. Subsequently the gas from the ullage space 3.3 of the reservoir 3.2 will be allowed to flow through the second duct section 3.5 into the gas main supply line 7. This causes a minor pressure drop in the ullage space 3.3, which is detected by the sensor 9. The measurement is transmitted to a control device (not shown for clarity reasons) which sends a command to the valve 9.1 in order to actuate opening movement. This, in turn, allows the liquid gas from the gas reservoir 3.2 to flow into the heat exchanger 3.9 in which the temperature of the liquid gas is raised, it may also at least partly evaporate. Since temperature of the liquefied gas is raised it will begin to flow back to the ~~reservoir 3.4~~ reservoir 3.2. This way the evaporation of the gas is increased and the pressure drop in the ullage space section 3.3 will be compensated. In case other type of heating device would be used its output power would be controlled by the pressure measurement sensor 9.

**Rewrite the paragraph beginning on page 11, line 4, to read as follows:**

The reservoir 3.2 is also provided with a return pipe 3.14, which leads from the liquid phase section of the reservoir back to the cargo tank 4. The return pipe 3.14 is provided with a valve 3.15 for controlling the flow of liquid gas. The valve 3.15 is responsive to the temperature in the ~~reservoir 3.4~~ reservoir 3.2, which is measure by a temperature measurement device 11 provided in connection with the gas ~~reservoir 3.4~~ reservoir 3.2. In case the temperature is too high the valve 3.15 is opened and the gas from the liquid phase section of the ~~reservoir 3.4~~ reservoir 3.2 will flow back to the cargo tank 4. The return flow will be compensated, when necessary, by feed from the cargo tank through the first duct section 3.4. Since the temperature in the cargo tank is about minus 163(C the liquid fed to the ~~reservoir 3.4~~ reservoir 3.2 will lower the temperature in the reservoir. In order to preheat the liquid gas fed to the reservoir and cool the returned portion of the gas. The flows are in heat transfer relation with each other by a first heat exchanger device 3.16. By maintaining proper temperature, preferably bout minus 100° C in the ~~reservoir 3.4~~ reservoir 3.2 as described above it is possible to facilitate separation of compounds contained in the gas, so that evaporation of desired known component or components of the gas occur and some part of the gas is returned to the cargo tank 4. Particularly heavier hydrocarbons may be separated from the gas so that the percentage of methane in the gas fed forward is increased. This arrangement is beneficial for the operation of the gas engines as the consumption device 5.